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Pd nanoflakes epitaxially grown on defect MoS₂ nanosheets for enhanced nitroarenes hydrogenation to anilines

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ABSTRACT

Hydrogenation of nitroarenes to anilines under mild conditions is attractive from both theoretical and practical viewpoints. Here, high-performance catalyst with layered Pd nanoparticles epitaxially growing on ultrathin MoS_2 nanosheets (Pd/ MoS_2) were prepared. It shows surprisingly high catalytic activity, selectivity and stability for hydrogenation of various nitroarenes to corresponding anilines; the turnover frequency is one or two magnitudes higher than conventional Pd-based catalysts. Surface sulfur vacancies are formed on MoS_2 nanosheets with low formation energy barrier. These S vacancies provide efficient positions for adsorbing Pd atoms, which enables facile cleavage of N–O bond as result of strong interfacial electron interaction that decreases activation energy by 0.41 eV in comparison with conventional Pd catalysts. In situ spectroscopy and DFT calculation results reveal a dual-site mechanism, in which surface Pd sites adsorb and dissociate H_2 into active H^* , and then readily reacts with nearby activated nitroarene to form aniline on interfacial Pd- MoS_2 sites.

1. Introduction

Nitroarene is harmful and toxic for human health, causing severe diseases such as methemoglobinemia [1,2]. The permissible exposure limit of 5 mg/m³ to human beings has been set for nitrobenzene (NB) in an 8 h-work day [1]. The strong electron affinity of -NO2 group makes them very difficult for oxidation. Thus, catalytic reduction of nitroarenes to anilines is a promising method, because anilines are important raw materials for the production of pharmaceutical, agrochemicals, pigments, dyes and polymers [3,4]. Currently, catalytic hydrogenation of NB and its derivatives to anilines have been industrially applied on a huge scale, and a variety of Pt or Pd-based catalysts have demonstrated to be effective for this reaction [5-13]. In these catalysts, reducible metal oxides, such as TiO2, CeO2 or FeOx, are usually employed as supports [5,7,9,14-17]. Atomically dispersed Pt on FeO_x shows high activity and strong chemospecificity towards the hydrogenation of functionalized nitroarenes [7]. Although some non-noble metal catalysts can activate nitroarenes, their activity and reaction rate are limited at mild conditions. Beller et al. and others reported a convenient method for preparation of stable Fe or Co oxides on carbon by pyrolysis of Fe or

Co complexes or metal-organic frameworks [18–23]. However, these catalysts are difficult to reach a turnover frequency (TOF) of 12000 mol/(mol·h) at temperature $\leq 80^{\circ}\text{C}$. Therefore, the intrinsic activity requests to be further improved by design of novel catalysts.

Defect engineering has been widely applied in transition metal dichalcogenides (TMDs) to tailor the electronic and geometrical factors [24-27]. Vacancies, known as a type of extremely delicate defect, are supposed to be effective and flexible in general catalytic modulation, which renders TMDs active for nitroarene reduction [28-30]. Schaak [29] fabricated WS₂ nanosheets with sulfur vacancy-rich basal planes and exhibited >99 % conversion of NB at 120 °C. Both MoS₂ [28] and MoSe₂ [30] nanosheets are also demonstrated to be effective for nitroarene reduction with NaBH₄. However, these pure TMDs showed very low intrinsic activity (< 20 mol/(mol·h), even under high reaction temperature or using strong reducing agent. Compared to traditional three-dimensional counterparts, two-dimensional (2D) TMDs nanosheets possess abundant surface active sites and defects, which are promising positions for anchoring metal sites due to strong metal-TMD interaction. Tsang et al. reported that sulfur vacancies in MoS2 monolayer facilitates the formation of Co-S-Mo interfacial sites that are the

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active sites of 4-methylphenol hydrodeoxygenation [31]. These vacancies make Pt monomers still maintain atomic dispersion even though the Pt content reaches 7.5 % on the MoS_2 nanosheets [32]. These researches encourage us to use ultrathin MoS_2 2D nanosheets with abundant S vacancies as support of metal species for catalyzing NB hydrogenation. Pure metal species, like Pd, has weak adsorption ability for NB, but is potential for activation of H_2 . We attempt to design a 'dual active site' catalyst, which activates H_2 and NB at spatially separated sites.

In comparison to metal sites, interfacial sites show higher adsorption and activation ability for oxygen-containing functional groups. It has been reported that Cu-O-Zn interface sites have much higher CO_2 adsorption energy than Cu^0 sites, indicative of a stronger activation ability for C=O groups [33,34]. The metal-support interfaces have been considered as crucial active sites in many reactions. Pt_1/α -MoC catalyst with interface structure is capable of selective hydrogenation of NB and its derivatives with high efficiency, even in the presence of CO pollutant [35]. Ultrathin CO_2 D nanosheets contain abundant CO_3 Nacional facilitate the formation of metal-support interfacial bonds. Here, layered CO_3 Pd nanoparticles (NPs) are synthesized on CO_3 NB hydrogenation. NB adsorbed on CO_3 ND interfacial sites is apt to react with surface CO_3 Hardward from CO_3 ND interfacial sites is apt to react with surface CO_3 ND hydrogenation on metallic Pd species, resulting in an extremely high NB hydrogenation activity under mild conditions.

2. Experimental

2.1. Materials

PdCl₂, NaBH₄ and Ce(NO₃)₂·6H₂O were purchased from Sinopharm Chemical Reagent Co., Ltd., China. (NH₄)₂Mo₂O₇·4H₂O and aniline were provided by Tianjin Chemical Reagent Co. Ltd, China. Thiourea was purchased from Aladdin. NaOH was purchased from Tianjin Kermel Chemical Reagent Co. Ltd, China. All the received chemicals were directly used without further purification.

2.2. Catalyst preparation

 MoS_2 nanosheets were prepared by a hydrothermal method [27], in which 2 mmol (NH₄)₂Mo₂O₇·4H₂O and 28 mmol thiourea were initially mixed in 70 mL water under vigorous stirring for 10 min. Subsequently, the solution was hydrothermally treated at 220 °C for 21 h. The obtained solid was centrifuged, washed and dried at 60 °C overnight. The as-prepared MoS₂ nanosheets possessed much higher BET surface area (29.1 $\,\mathrm{m^2/g}$), while the commercially obtained bulk MoS₂ (b-MoS₂, Sinopharm Chemical Reagent Co., Ltd., China) had only 7.1 $\,\mathrm{m^2/g}$ surface area

The nanoporous Mo_2C nanowires were synthesized by a previously reported method [36]. 2.48 g $(NH_4)_2Mo_2O_7\cdot 4H_2O$ and 3.20 g aniline were mixed in 40 mL water, followed by the addition of HCl aqueous solution (1.0 mol/L) until the formation of white precipitate at pH 4–5. After stirring at 50 °C for 6 h, the collected solid was centrifugated, washed, dried at 80 °C overnight, and annealed at 850 °C for 12 h in flowing Ar atmosphere.

CeO $_2$ with rod shape was prepared by a hydrothermal method. 4.5 mmol Ce(NO $_3$) $_2$ ·6H $_2$ O was initially dispersed into 90 mL NaOH solution (5 mol/L) under stirring for 10 min at room temperature. Subsequently, the solid sample was centrifugated with water, dried at 80 °C overnight and calcined at 400 °C for 4 h.

For the preparation of Pd/MoS_2 catalyst (3 wt% Pd content as an example), 1 mL H_2PdCl_4 solution (0.226 mol/L) was dissolved in 10 mL H_2O under vigorous stirring, followed by the addition of 0.8 g MoS_2 . After stirring for 1 h, 13.56 mL NaBH₄ (0.25 mol/L) solution was dripped into above solution with continuous stirring for 1 h. Subsequently, the solid sample was repeatedly centrifuged, washed and dried at 80 °C overnight. The other supported Pd catalysts were synthesized with the

same method as above.

2.3. Catalyst characterization

Inductively coupled plasma atomic emission spectroscopy (ICP-OES, Optima 2100DV, PerkinElmer) was conducted to measure Pd content, and their results are displayed in Table S1. N2 adsorption-desorption isotherms were performed at −196 °C on a Micromeritics TriStar 3000 instrument. Before its measurement, the catalysts sample was pretreated at 200 °C for 8 h. X-ray powder diffractometer (XRD) was taken on Rigaku MiniFlex II desktop X-ray diffractometer using Cu Kα radiation at 40 kV and 40 mA. The images of transmission electron microscopy (TEM), high resolution TEM (HR-TEM) and high-angle annular darkfield scanning TEM (HAADF-STEM) were performed on a JEM-2011F system electron microscope at 200 kV with a field emission gun. Prior to its measurement, the sample was dispersed in ethanol by sonication, and deposited on carbon-coated copper grids. X-ray photoelectron spectroscopy (XPS) was conducted on Kratos AXIS ULTRA DLD spectrometer using Al Kα radiation. Raman spectra was performed in HORIBA Scientific LABRAM HR Evolution with an excitation wavelength of 532 nm. Electron paramagnetic resonance (EPR) spectra was measured on EMXPLUS10/12 X-band spectrometer at room temperature. In situ diffuse reflection Fourier transform infrared spectra (DRIFTS) was conducted on FTIR spectrophotometer (Nicolet Is10) using a SMART collector and an MCT detector cooled in liquid N2. Typically, 40 mg catalyst slice was pretreated at 300 °C for 2 h in a H₂/ Ar gas (20 mL/min), and subsequently cooled down into room temperature in flowing Ar gas. Once NB was introduced into the catalyst surface, DRIFTS spectra was immediately used to monitor its adsorption to saturated state. With increasing temperature to 80 °C, the adsorbed NB gradually desorbed from catalyst surface. Once the DRIFTS spectra of adsorbed NB kept stable at 80 °C, H2 (20 mL/min) was purged into the system and the DRIFTS spectra were detected simultaneously.

2.4. Catalyst evaluation

The catalytic reactions were performed in a Teflon-lined stainless steel autoclave (NS-10-316L, Anhui Kemi Machinery Technology Co., Ltd.). 10 mmol nitrobenzene and 0.05 g catalyst were typically loaded into the reactor. After been purged with H2 for five times, the reactor was pressured into 4.0 MPa H₂, heated to 80 °C, and kept for desired time. Once the reaction was finished, the reaction system would been rapidly cooled down in an ice-water bath. Before product analysis, the liquids products were diluted with 20 mL ethanol, and separated with catalysts by centrifugation. The collected products were analyzed by gas chromatography (GC, Shimadzu GC-2010) with a flame ionization detector using a DB-1 capillary column (60 m \times 0.25 mm \times 0.25 μ m). All the products were identified by standard chemicals and GC-MS. For the determination of apparent activation energy and turnover frequency (TOF), the conversion of nitrobenzene was generally kept below 20 %. TOF was calculated based on surface Pd atoms, which can be obtained according to the equation that Pd dispersion multiplies by Pd amount.

$$TOF = \frac{\textit{Mole number of converted nitrobenzene}}{\textit{Number of surface Pd atoms} \times \textit{reation time}}$$

Pd dispersion is calculated by the equation $D = \frac{6 \times V}{6 \times d}$, in which V is the volume of per Pd atom (0.0147 nm³), a is the surface area per Pd atom (0.0793 nm²), and d refers to Pd average particle size in nm from TEM counting [37].

For reusability tests, the spent catalyst was repeatedly washed with ethanol, collected by centrifugation, and dried at 80 $^{\circ}$ C overnight. Subsequently, the spent catalyst was performed according to normal procedure.

2.5. Density functional theory (DFT) calculation method

Vienna *ab initio* simulation package (VASP) was used to perform plane-wave-based periodic DFT calculations [38–40]. Perdew, Burke, and Ernzerhof (PBE) functional was employed to describe exchange and correlation energy. The electron-ion interactions were treated by projector augmented wave (PAW) setups [41,42]. According to TEM results, the most exposed Pd (1 1 1) facet was simulated with 5 \times 5 four-layer supercell. The most exposed MoS $_2$ (0 0 2) surface was modelled by 5 \times 4 three-layer supercell, in which S vacancies were built by the removal of two atoms from 20 surface S atoms on top layer to select low formation energy. The thickness of vacuum layer was 20 Å along the direction perpendicular to Pd (1 1 1) or MoS $_2$ (0 0 2) slabs to avoid artificial interactions between the slab and its periodic images. The Pd $_{15}/\text{MoS}_2$ interface was modeled with a 15 atoms Pd cluster bound to the above MoS $_2$ (0 0 2) model with S vacancies.

Adsorption energy (E_{ads}) was defined as the energy difference of the most stable structure, relative to clean slab (E_{slab}) and substrate molecule (E_{sub}), which is calculated by the equation $E_{ads} = E_{sub/slab} - E_{slab} - E_{sub}$. The transition states (TSs) were probed by climbing image nudged elastic band (CI-NEB) method [43,44], which were further verified by the presence of a single imaginary vibrational mode in frequency analysis. Activation energy (E_a) of an elementary reaction was defined by energy difference between TS and initial state (IS), while reaction energy (E_r) was defined by energy difference between final state (FS) and IS.

3. Results and discussions

3.1. Catalyst characterization

HR-TEM images of Pd/MoS $_2$ catalyst show that MoS $_2$ has a nanosheet morphology with a thickness of 3–5 layers (Fig. 1). The ultrathin MoS $_2$ nanosheet-supported Pd possessed much higher surface area than bulk MoS $_2$ -supported Pd catalyst (Pd/b-MoS $_2$) (23.1 m $_2$ /g vs. 4.2 m $_2$ /g) (Table S1). A typical lattice spacing of 0.65 nm was observed in the HR-

TEM images, which is ascribed to the (002) crystalline plane of MoS_2 [27,45]. Pd NPs are uniformly dispersed on the surface of MoS_2 nanosheets (Fig. 1h), and the average particle size is about 3.0 nm (Fig. 1d). The most exposed facet of Pd NPs is (111) crystalline plane [46], as substantiated by the lattice spacing of 0.23 nm of fcc symmetry (Fig. 1b and Fig. S1). Notably, Pd species deposited on MoS_2 nanosheets formed small-layered Pd NPs, which had an average thickness of 5–8 at. layers (2–3 nm), as estimated from edge-on images of Pd NPs. Crystal structure analysis indicates that the Pd NPs strongly aligned with the (002) planes of MoS_2 support. The strong interface interaction between Pd and MoS_2 nanosheets enables Pd monomers to epitaxially grow with a relatively low speed along the direction of (111) orientation, rather than rapid aggregation to form irregular nanocrystals and random orientations [46]. The HAADF-STEM and elemental mappings confirm that Pd, S and Mo species are all homogenously dispersed in the MoS_2 nanosheets.

Pd/b-MoS₂ shows larger Pd particle size and wider size distribution, although its Pd content is similar to that of Pd/MoS₂ (Fig. S2). This may due to a weaker interaction between Pd species and b-MoS₂. In the cases of Pd/Mo₂C and Pd/CeO₂, the Pd NPs are also highly dispersed on the supports, and thus, have small sizes (Fig. S3 and Fig. S4). No diffraction peaks characteristic of Pd species were detected by XRD technique for all the catalysts (Fig. S5). The intense diffraction peaks at 14.3°, 32.7°, 39.5°, 49.8° and 58.4° in the XRD pattern of Pd/b-MoS2 are indexed to the (002), (100), (103), (105) and (110) crystalline planes of 2 H-MoS₂ (JCPDS No. 01-073-1508). However, these diffraction peaks were significantly broadened and became much more diffuse for Pd/MoS₂, giving another piece of evidence for considerably thinning of MoS2 layer. Compared to conventional b-MoS2, MoS2 nanosheets shows a smaller 20 value at the (002) plane diffraction peak, suggesting an expanded interlayer spacing between S-Mo-S layers, consistent with the above HR-TEM results.

Two obvious peaks centered at 380 and 407 cm $^{-1}$ were observed in the Raman spectra (Fig. 2a). These two peaks are ascribed to the in-plane $E_{2\,g}^1$ and out-of-plane A_g^1 vibration modes of MoS $_2$ [24,47]. The $E_{2\,g}^1$ peak of MoS $_2$ nanosheets distinctly redshifted and broadened, compared to that of b-MoS $_2$. This indicates the softening of Mo-S phonon mode and

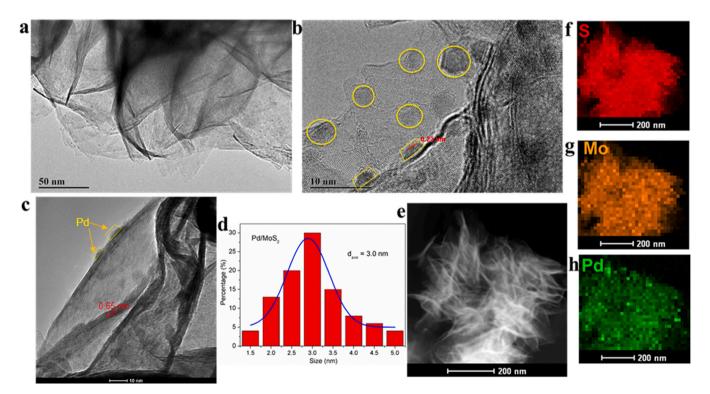


Fig. 1. (a) TEM and (b,c) HR-TEM images, (d) Pd particle size distribution, (e) HAADF-STEM image and elemental mappings of (f) S, (g) Mo and (h) Pd on Pd/MoS₂.

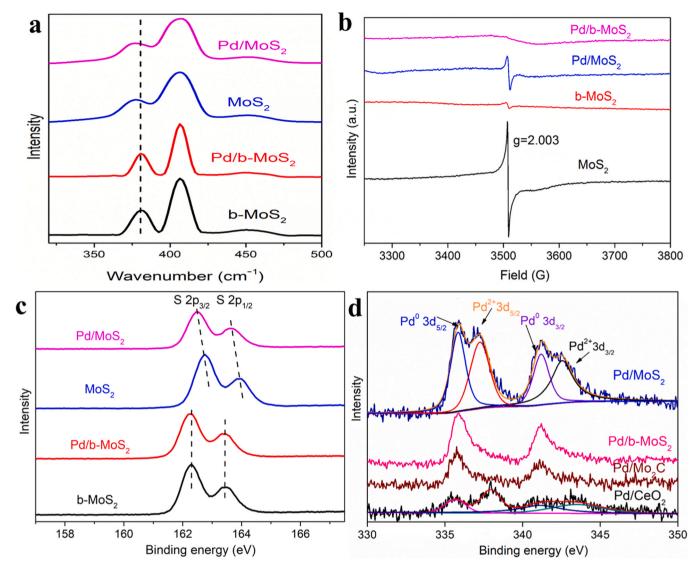


Fig. 2. (a) Raman spectra, (b) EPR spectra, and (c) S 2p and (d) Pd 3d XPS spectra of various catalysts.

basal plane, as a result of a decrease of Mo–S chemical bonds number and an increase of in-plane S vacancies. The presence of abundant S vacancies in MoS₂ nanosheets is further corroborated by the observation of an intense peak at g = 2.003 in its EPR spectra (Fig. 2b) [24], as this peak is corresponding to the Mo–S dangling bonds originating from the single S-vacancies on MoS₂ surface. Compared to MoS₂ nanosheets, moderate decrease of peak intensity was detected on Pd/MoS₂, suggesting that the introduced Pd species occupied some S vacancies. The very weak peaks in the EPR spectra of b-MoS₂ indicate that it has small numbers of S vacancies.

In the S 2p XPS spectra (Fig. 2c), two distinct peaks were detected at about 162.3 and 163.4 eV, which are attributed to S^{2-} in MoS $_2$ [26,48]. Meanwhile, two symmetrical peaks centered at 229 and 232.3 eV are assigned to Mo $^{4+}$ in MoS $_2$ (Fig. S6) [24]. The surface S vacancy concentrations, as determined by XPS spectra in terms of the S: Mo ratio, in commercial b-MoS $_2$ and Pd/b-MoS $_2$ are 0.9 % and 0.8 %, respectively. Comparatively, those in MoS $_2$ nanosheets and Pd/MoS $_2$ reaches 12.1 % and 10.6 %, suggesting the presence of large amounts of S vacancies, consistent well with the EPR results.

In the Pd 3d XPS spectra of reduced Pd/b-MoS $_2$ and Pd/Mo $_2$ C (Fig. 2d), the intense symmetrical peaks at 335.9 and 341.2 eV are assigned to Pd 0 3d $_{5/2}$ and 3d $_{3/2}$, respectively [46,49]. Another two peaks were observed at 337.2 and 342.6 eV in the spectra of Pd/MoS $_2$ and

Pd/CeO₂, which are attributed to Pd²⁺ [46,49,50]. It has been reported that the presence of Pd²⁺ indicated the probable formation of Pd–O–Ce bond due to the strong interfacial interaction between Pd and CeO₂ [49]. Compared to MoS₂, addition of Pd induced a remarkable shift of S 2p peak toward low binding energy, suggesting that MoS₂ obtained electrons that probably derived from Pd. Meanwhile, the presence of Pd²⁺ peak at high binding energy was due to electron transfer from Pd⁰ into S²⁻. The XPS results confirm the existence of strong interfacial interaction between Pd species and MoS₂ nanosheets that possess a substantial number of S vacancies, and thus, facilitate the formation of interfacial Pd–S–Mo bonds.

S vacancies can be created by removing surface S atoms during DFT modelling (Fig. S7). DFT calculation results reveal that the S vacancy formation energy is 0.33 eV on MoS₂, and Pd–S–Mo bonds are formed through hybridization of Pd 3d orbitals and neighboring S 2p orbitals of MoS₂ with which can stabilize the loaded Pd on the MoS₂ surface through Pd–S interaction. The stabilization energy was calculated as high as -7.4 eV per cluster. As a result, the shift and aggregation of Pd species were prevented [51]. The optimized structure of Pd/MoS₂ is shown in Fig. 3a. The average distance of Pd–S bond is ca. 2.3 Å, giving another piece of evidence for the existence of strong interfacial interaction between interfacial Pd and S atoms. In addition, Pd atoms can partially occupy S vacancy sites to create new Pd–Mo bonds with a

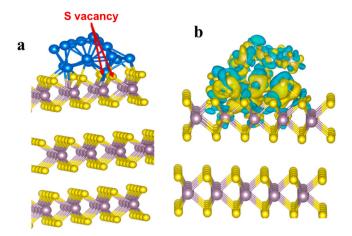


Fig. 3. (a) Atomic configuration of DFT calculation-optimized structure, and (b) calculated charge-density differences on Pd_{15}/MoS_2 model (blue, yellow, and brown balls represent Pd, S, and Mo atoms, respectively).

length of ca. 2.70 Å, consistent with ERP spectra and XPS results. In contrast, Pd clusters can only form Pd-S bonds in bulk MoS $_2$ with small numbers of S vacancies (Fig. S7c).

The charge density analysis can give information on the distribution

of electrons, which is readily acquired from the wave functions by DFT calculations. Charge-density differences provides direct visual evidence on electron interaction via interfacial charge transfer between different materials. The charge-density differences (Δρ) on Pd₁₅/MoS₂ were calculated by the equation: $\Delta \rho = \rho(Pd_{15}/MoS_2) - \rho(Pd_{15}) - \rho(MoS_2)$, where $\rho(Pd_{15}/MoS_2)$, $\rho(Pd_{15})$, and $\rho(MoS_2)$ are the charge-densities of Pd₁₅/MoS₂, Pd₁₅, and MoS₂, respectively. Fig. 3b displays the chargedensity differences of Pd/MoS2 model, with yellow and blue representing charge accumulation and charge depletion, respectively. The electron densities on the interfacial Pd and MoS2 were significantly increased and seriously overlapped between the interfaces. In addition, the subsurface Mo atoms also had electronic interaction with interfacial Pd atoms. The electron density of surface Pd species moves toward Pd-MoS₂ interface, demonstrating that the interaction between Pd clusters and surface MoS₂ sites are very strong [52]. Notably, nearly no obvious interaction is observed between Pd clusters and the subsurface MoS₂. Obviously, ultrathin nanosheet structure of MoS2 is crucial for the formation of more Pd-MoS2 interfacial sites due to the presence of large numbers of surface S vacancies.

3.2. Catalytic performance

Fig. 4a shows the catalytic results of various catalysts for NB hydrogenation to aniline at 80 $^{\circ}$ C and 4 MPa H₂ in the absence of solvent. Pd/b-MoS₂ and Pd/Mo₂C exhibited very low NB conversions of only 3.1

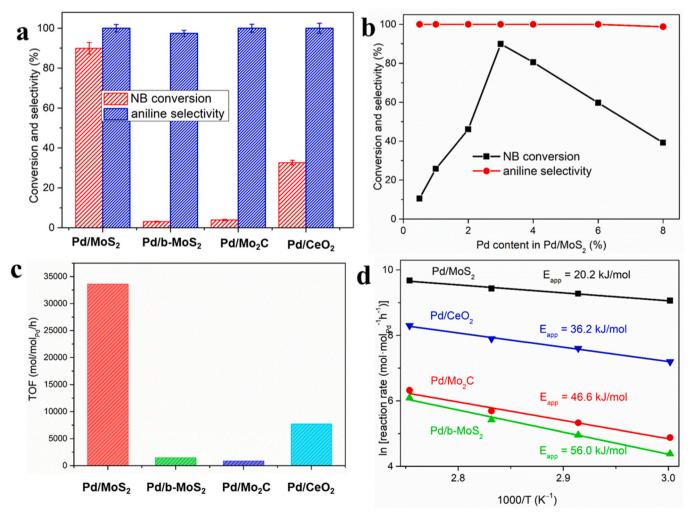


Fig. 4. (a) NB hydrogenation results over various catalysts; (b) effect of Pd content on the catalytic performance of Pd/MoS₂ for NB hydrogenation; (c) TOF value over various catalysts at 80 °C. (d) Kinetic behaviour and apparent activation energies of NB hydrogenation over various catalysts. Reaction conditions: 10 mmol NB, 0.005 g catalyst, 80 °C, 4 MPa H₂, 1 h. The reaction conditions for Fig. 4d are listed in Table S2.

% and 3.9 % respectively, whereas Pd/MoS_2 gave a NB conversion as high as 89.9 %, despite that all the catalysts displayed aniline selectivity > 97 %. The catalytic activity of MoS_2 nanosheets alone was also evaluated. However, the conversion of NB was only 0.2 %. Pd/CeO_2 is a well-known highly active catalyst for NB hydrogenation [5,53], but it also obtained low conversion (32.6 %) at the same condition, demonstrating the superior catalytic performance of Pd/MoS_2 .

Fig. 4b shows that the optimal Pd content in Pd/MoS₂ catalyst is 3 wt % in theoretic content (2.59 wt% actual content by ICP). NB conversion improved with increasing Pd content from 0.5 wt% to 3 wt%. When Pd content was 3 wt%, Pd/MoS2 achieved the best performance, up to 89.9 % NB conversion. An increase of Pd content can remarkably improve Pd active sites and promote the activity. However, too high Pd content (>3 wt%) tended to cause the agglomeration of Pd particle, decreased Pd dispersion, and thus diminished the number of interfacial Pd active sites, resulting in the decline of NB conversion. The correlation between TOF value with Pd content is displayed in Fig. S8. Similar trend was observed in the cases of TOF or NB conversion with Pd content. The TOF value also increased with Pd content, and reached the highest for 3 wt% Pd/MoS₂. The effect of reaction time on catalytic performance of NB hydrogenation was investigated on Pd/MoS₂ and the result is illustrated in Fig. S9. NB conversion gradually enhanced with increasing reaction time. Both NB conversion and aniline selectivity reached 100 % for 1.5 h.

The reusability tests of Pd/MoS2 were performed, and the reaction result is displayed in Fig. S10a. No discernible decrease in NB conversion and aniline selectivity was observed after six recycle tests. ICP result indicated that no obvious Pd and Mo species (< 0.1 wt%) were leached into solution after reusability tests. TEM images of spent Pd/MoS2 (Fig. S11a,b) showed that MoS2 nanosheet structure was well maintained. The spent Pd/MoS2 catalyst presents almost no aggregation of Pd NPs and the Pd-MoS₂ interface can still be remained. Additionally, the Raman, EPR and XPS spectra (Fig. S11c-e) of spent Pd/MoS2 behaved similar to the fresh sample, confirming the robust chemical structure and stable S vacancies. Compared to fresh Pd/MoS2 (52.0 %), a slight increase of $Pd^{2+}/(Pd^0+Pd^{2+})$ ratio (55.1 %) on spent sample is probably due to Pd⁰ oxidation during post-treatment after recycle test. Because catalyst deactivation may be masked at high conversion of NB, the reusability tests were further conducted for Pd/MoS2 at low conversion (48.9 %). Similar case (Fig. S10b) was observed that the conversion of NB and aniline selectivity was maintained within six runs, demonstrating the excellent stability of Pd/MoS₂.

The intrinsic activity of various catalysts as manifested by TOF was normalized to surface Pd. Pd/b-MoS $_2$ obtained a TOF value of 1461 mol/mol $_{Pd}$ /h. Pd/CeO $_2$, as expected, gave a much higher TOF value of 7739 mol/mol $_{Pd}$ /h at 80 °C, which is similar to the reported result [5,53]. Excitingly, Pd/MoS $_2$ displayed an extraordinarily high TOF value of 33617 mol/mol $_{Pd}$ /h at 80 °C. To the best of our knowledge, such a TOF value has rarely been achieved [7,10,19,21,35]. It is generally one or two magnitudes higher than previously reported catalysts, and even outperforms single atom catalysts such as Pt $_1$ /FeO $_1$ [7], Pt $_1$ /mpg-C $_3$ N $_4$ [11], Ru $_1$ Ni/Al $_2$ O $_3$ [54], Ir $_1$ Mo $_1$ /TiO $_2$ [55] and Co $_1$ /Graphene [56].

The effect of external diffusion was checked by varying the stirring speed between 600 and 1500 rpm. As shown in Fig. S12, the conversion of NB enhanced with increasing stirring speed up to 1200 rpm. However, no further enhancement of NB conversion was observed with the stirring rate of 1500 rpm. Thus, the stirring speed was fixed at 1200 rpm, which can efficiently remove the external diffusion limitation. The internal diffusion effect is mainly controlled by catalyst size. For small catalyst particle size of Pd/MoS $_2$ (ca. 50 μ m), an inter-particle diffusion resistance can be usually excluded for tank reactor. Additionally, a further decline in particle size by grinding did not improve NB conversion, indicating the absence of internal diffusion limitations. Thus, internal and external diffusion limitations can be neglected in the intrinsic regime, and the applied reaction condition was suitable for

kinetic study. The kinetics studies (Fig. 4d and Table S2) show that the apparent activation energy (E_{app}) on Pd/MoS₂ is 20.2 kJ/mol, being much lower than those on Pd/b-MoS₂ (56 kJ/mol), Pd/CeO₂ (36.2 kJ/mol) and Pd/Mo₂C (46.6 kJ/mol). This accounts for the high activity of Pd/MoS₂.

The outstanding catalytic performance of Pd/MoS₂ is further substantiated by its tolerance to a variety of NB-based compounds, including both electron-donating (methyl, methoxy, and phenolic hydroxy) and electron-withdrawing (hydroxymethy, carboxyl, halogen, amino) groups-substituted NBs (Table 1). More interestingly,

Table 1
Catalytic results for hydrogenation of various substituted nitroarenes on Pd/MoS.

Substrate	Product	Reaction time (h)	Conv. (%)	Sel. (%)
NO ₂	NH ₂	1.5	100	>99.9
NO ₂	NH ₂	1.5	100	>99.9
NO ₂	NH ₂	2	97.8	99.1
NO ₂	NH ₂	1.5	96.5	96.9
NO ₂	CH ₃ O NH ₂	1.5	99.8	95.9
HOOC NO2	NH ₂	2	99.6	98.7
NO ₂	NH ₂	2	99.1	96.3
NO ₂	NH ₂	2	96.5	98.0
NO ₂	NH ₂	2	100	97.8
NO ₂	NH ₂	2	99.7	96.9
NO ₂	NH ₂	2	100	95.1
NC NO2	NC NH ₂	2	100	96.8
NO ₂	NII ₂	2	100	97.9

Reaction conditions: 10 mmol substrate, 0.005 g catalyst, 80 $^{\circ}\text{C},$ 4 MPa $H_2,$ 1.5 or 2 h.

nitroarenes with easily reducible alkene, nitrile and/or aldehyde functional groups can be selectively converted into corresponding anilines, although it is a challenge [18,19]. In all studied cases, the functionalized anilines selectivity is higher than 95 % along with the nitroarene conversion >96 % within 2 h.

3.3. Reaction mechanism

Fig. 5a shows the in situ DRIFTS of Pd/b-MoS2 and Pd/MoS2 for hydrogenation of NB at 80 $^{\circ}$ C. Two typical bands were detected at 1348 and 1527 cm⁻¹ on the both samples. These two bands are ascribed to the N=O stretching vibrations of adsorbed NB [57,58]. No significant change was observed with the reaction time on Pd/b-MoS₂, supporting its very low activity. In contrast, these two bands obviously declined at 5 min on Pd/MoS₂. Simultaneously, another two bands appeared at 1484 and 1310 cm⁻¹, which are attributed to the N=O and C-N stretching vibrations of nitrosobenzene [59]. In addition, the peaks characteristic of phenylhydroxylamine were also discerned at 1492 and 1246 cm⁻¹. Further increase of the reaction time to 30 min led to the new bands at 1622 ($\delta(NH_2)$), 1601 ($\delta(NH_2)$), 1500 ($\nu(C-N)$), 1273 (ν (C-N)) and 1174 cm $^{-1}$ (ν (C-H)) at the expense of those for nitrosobenzene and phenylhydroxylamine. These new bands are assigned to the vibrations of adsorbed aniline [60]. The in situ DRIFTS results of Pd/MoS₂ not only demonstrate its extraordinarily high activity, but also reveal that NB is hydrogenated to aniline via the C₆H₅NO and C₆H₅NHOH intermediates (Fig. S13).

DFT calculations show that NB is very difficult to be chemically adsorbed on b-MoS₂ or MoS₂ surface (Fig. S14), but it can be adsorbed on Pd (111) plane in parallel pattern through the formation of six C-Pt bonds with an adsorption energy of -1.00 eV (Table S3). Notably, the nitro group cannot effectively bind to Pd (111) surface in a vertical way, as the adsorption energy of $-0.41\,$ eV is too weak to cause NB activation. In addition, NB can also be strongly adsorbed on Pd₁₅/MoS₂ (002) interface in parallel pattern (adsorption energy of -1.21 eV), due to the contribution from nitro group in the formation of strong N-O-Pd-S-Mo bond (Table S4). Obviously, the interfacial Pd-S-Mo bond can rapidly activate nitro group and promote its conversion. The adsorption structures of other possible intermediates were also calculated, and the results are displayed in Tables S3 and S4. Generally, their adsorption energies on Pd (111) surface are lower than those on Pd₁₅/ MoS₂ interface model, which is attributed to the increased electron densities around Pd-MoS2 interfacial area and Pd-occupied sulfur vacancies to induce electronic interaction from Pd-Mo bonds.

The H^* formation is vital for hydrogenation reaction [61,62]. Its rapid generation, diffusion and maximizing the coverage on active sites can greatly increase the intrinsic rate of NB reduction. H_2 dissociation is

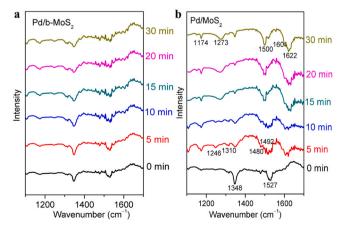


Fig. 5. In situ DRIFTS spectra of NB hydrogenation over (a) $Pd/b-MoS_2$ and (b) Pd/MoS_2 .

very easy to occur on Pd (111) plane by overcoming an activation energy barrier of only 0.27 eV (Table S5). The activation energy is further decreased to 0.19 eV on Pd_{15}/MoS_2 model (Table S6), because Pd step and corner sites in Pd_{15} cluster are more active. Notably, these surface Pd sites also display higher catalytic activity than interfacial Pd sites for H_2 activation.

In situ DRIFTS results show that NB is hydrogenated into aniline by a direct pathway as the C₆H₅NO and C₆H₅NHOH intermediates were detected. Fig. 6 and Table S5 list the related elementary reactions in detail. The C₆H₅NO₂* adsorbed on Pd (111) surface is initially hydrogenated to C₆H₅NO₂H* with an O-H bond length of 1.45 Å (TS1), which requires an activation energy barrier of 0.68 eV. The formed C₆H₅NO₂H* is further attacked by nearby H* to generate C₆H₅NO* and H₂O* with an activation energy barrier of 0.54 eV. This step is strongly exothermic with a released heat of -0.99 eV·H₂O* as a byproduct is weakly adsorbed on the top Pd site (adsorption energy of -0.28 eV). Thus, it can be easily desorbed from the Pd sites. The formed C₆H₅NO* species is subsequently hydrogenated into C₆H₅NOH* by surmounting a low activation barrier of 0.52 eV. The C₆H₅NOH* species is then sequentially hydrogenated to C₆H₅NHOH* by overcoming a high energy barrier of 0.93 eV due to serious geometric constraint effect. The formed C₆H₅NHOH* can dissociate into C₆H₅NH* and OH* by breaking robust N-O bond. This step needs to overcome a very high energy barrier of 1.25 eV and is exothermic by -0.11 eV, which is the rate-determining step. Finally, aniline is formed by the hydrogenation of C₆H₅NH* with a relatively high energy barrier of 0.85 eV. Notably, NB hydrogenation to aniline is strongly exothermic in thermodynamics, which is beneficial to achieving of high aniline selectivity.

The NB hydrogenation reaction pathway on Pd_{15}/MoS_2 interfacial model was also investigated by DFT calculations (Fig. 6 and Table S6). The activated NB is rapidly hydrogenated to $C_6H_5NO_2H^*$ with an activation energy barrier of 0.43 eV. Upon hydrogenative dehydroxylation, $C_6H_5NO_2H^*$ is transformed into $C_6H_5NO^*$ species ($E_a=0.32$ eV), which undergoes consecutive hydrogenation to yield C_6H_5NHOH ($E_a=0.66$ eV). The rate-determining step of $C_6H_5NHOH^*$ dehydroxylation requires an activation energy barrier of 0.82 eV, which is much lower than that on Pd (111) model. Unlike on Pd (111) surface, where $C_6H_5NHOH^*$ suffers a considerable rotation of N-O axes in N-OH bond scission, a small structural change at Pd_{15}/MoS_2 interface contributes to the obvious decline of activation energy. The generated $C_6H_5NH^*$ is finally hydrogenated to the aimed product of $C_6H_5NH_2$ by overcoming an activation energy barrier of 0.57 eV. Compared to Pd (111), Pd_{15}/MoS_2 interfacial model shows remarkably lower activation energy

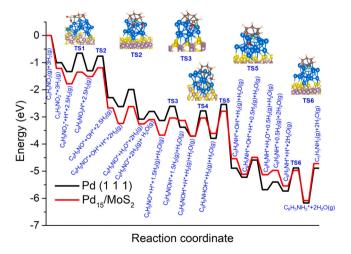


Fig. 6. Potential energy diagram for the hydrogenation of NB on Pd (111) and (b) Pd_{15}/MoS_2 . "TS" refers to the transition state. The blue, yellow, brown, black, green, red and white balls represent Pd, S, Mo, C, N, O and H atoms, respectively.

barriers in most elementary reactions, which is due to the strong interfacial interaction that increases electron density around Pd. Location of Pd atoms at the sulfur vacancies sites leads to formation of Pd—Mo bond and enhances interfacial Pd electron density. Pd—S—Mo interface bonds facilitates the adsorption and activation of N=O group, and thus, lowering its hydrogenation activation energy barrier. On Pd₁₅/MoS₂ interface, the stabilization of reaction intermediates involved in NB hydrogenation requires a synergetic action of Pd, S, and Mo sites, and the Pd-MoS₂ interface likely provides multiple active sites for the reaction.

Previous reports [11,14,58] have shown that high aniline selectivity was achieved for NB hydrogenation on noble metal catalysts. DFT calculations demonstrated that nitrobenzene is hydrogenated to produce nitrosobenzene (C_6H_5NO), hydroxylaniline (C_6H_5NHOH) and aniline successively, with strongly exothermic properties on both Pd (1 1 1) and Pd₁₅/MoS₂ models (Fig. 6). Thus, this reaction is thermodynamically driven full hydrogenation and produces aniline with high selectivity on Pd surface and Pd-MoS₂ interfacial sites.

The results of DFT calculations and in situ DRIFTS of Pd/MoS $_2$ for NB hydrogenation confirm that NB is hydrogenated into aniline with a direct pathway on both the Pd (111) and Pd $_{15}$ /MoS $_2$ models. Notably, NB hydrogenation follows a dual-site mechanism on Pd/MoS $_2$, where surface Pd sites preferentially adsorb and activate H $_2$, while interfacial Pd-MoS $_2$ sites tend to activate NB molecules and promote the hydrogenation with H*. Ultrathin MoS $_2$ nanosheets possess large numbers of S vacancies that facilitate anchoring of Pd atoms and enhance interfacial electron interaction, and as a consequence, leading to an exciting catalytic performance.

4. Conclusions

Pd nanoflakes epitaxially grown on MoS2 nanosheets show significantly high catalytic activity in nitroarenes hydrogenation to anilines; the TOF reaches 33617 mol/mol_{Pd}/h at 80 °C, being higher than reported values by one or two magnitudes. More interestingly, Pd/MoS2 displays extensive substrate tolerance and excellent structural stability during recycling tests. MoS₂ nanosheets possess large numbers of sulfur vacancies as a result of low formation energy barrier of S vacancies, which have strong interfacial interactions with Pd NPs. A part of Pd atoms are adsorbed on the sulfur vacancies, forming Pd-Mo bonds. In situ DRIFTS results reveal that NB is directly hydrogenated into aniline via the formation of C₆H₅NO and C₆H₅NHOH intermediates. DFT calculations confirm that surface Pd sites can activate and dissociate H₂, whereas interfacial Pd sites facilitate NB adsorption and activation. The Pd-MoS2 interfacial sites as main active species enable the N-O bond cleavage by decreasing the activation energy barrier of 0.41 eV. This work highlights the crucial role of sulfur vacancies in forming interfacial active sites structure and contributes to the design of high-performance supported metal catalysts.

CRediT authorship contribution statement

Weibin Fan: Writing – review & editing, Supervision, Resources, Conceptualization. Xiangyu Jia: Methodology, Investigation. Jiamin Wang: Methodology, Investigation. Xiaoming Li: Methodology, Investigation. Mei Dong: Resources, Project administration. Shanhui Zhu: Writing – original draft, Software, Funding acquisition, Data curation, Conceptualization. Zexiang Lv: Methodology, Investigation.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Data availability

Data will be made available on request.

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Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at doi:10.1016/j.apcatb.2024.123958.

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